



Approved baseline and monitoring methodology AM0034

“Catalytic reduction of N₂O inside the ammonia burner of nitric acid plants”

I. SOURCE, DEFINITIONS AND APPLICABILITY

Source

This baseline and monitoring methodology is based on the following proposed new methodology:

- NM0143 “Baseline Methodology for the Catalytic Reduction of N₂O inside the Ammonia Burner of Nitric Acid Plants” submitted by N serve nvironmental Services GMBH, with components from NM0164 “Baseline methodology for project activities involving secondary catalytic N₂O abatement at an existing nitric acid plant” prepared by MGM International Ltd.

This methodology also refers to the approved methodology:

- AM0028 “Catalytic N₂O destruction in the tail gas of nitric acid plants”.

This methodology also refers to the latest approved version of the following tool(s):

- “Tool for the demonstration and assessment of additionality”.

For more information regarding the proposals and the tools, as well as their consideration by the Executive Board, please refer to <<http://cdm.unfccc.int/goto/MPappmeth>>.

Summary

Nitric Acid (HNO₃) is produced through the oxidisation of ammonia (NH₃) on precious *metal catalyst gauze* in the ammonia burner of a nitric acid plant. Nitrous Oxide (N₂O) is a by-product gas produced in the manufacture of nitric acid. Waste N₂O from nitric acid production is typically released into the atmosphere, as it does not have any economic value or toxicity at emission levels typical of nitric acid manufacture.

Nitric acid plants operate on discrete production runs called “campaigns”. The start of a campaign is characterized by the installation of a new set of primary catalyst gauzes in the oxidation reactor. A set of precious *metal gauzes* (generally a platinum-rhodium alloy) is designed to operate either for a specific number of days or for a specific output of nitric acid. Over time the gauze decomposes and become less selective for the formation of NO. The production efficiency, therefore, drops and the formation of by-products increases. At the end of the design operating life of each gauze, the nitric acid plant is shut down and the gauze is replaced by new gauze. The period of time beginning from the installation of a new gauze pack until the subsequent plant shut down is defined as a *campaign*.

This methodology covers project activities involving the installation of a dedicated N₂O abatement catalyst inside the ammonia burner of a nitric acid plant that catalytically reduces N₂O, once it has been formed in the Ammonia Oxidation Reactor.

Baseline emissions are determined by measuring N₂O concentration and total flow rate in the tail gas of the nitric acid plant. These measurements are for the duration of one entire campaign, and are used to determine a plant-specific baseline emissions factor (tN₂O/t HNO₃). A permitted range for parameters that influence the level of N₂O formation (e.g., ammonia, ammonia-air input, temperature



and pressure) is established during the baseline campaign to define the permitted range for which emission reduction credits can be claimed during the crediting period. These permitted ranges must also be demonstrated to be within the specifications of the plant.

During the project activity, the measurements of N₂O and other parameters are carried out on a continuous basis and new emissions factors are established for each project campaign.

Total emission reductions for the project for a specific campaign are calculated by subtracting the project emissions factor from the baseline emissions factor and multiplying the result by the number of tonnes of nitric acid produced in the particular campaign.

The methodology requires the installation of a complete N₂O monitoring system that includes both a gas volume flow meter and an infrared gas analyser to determine the concentration of N₂O. The total mass of N₂O emissions is determined by multiplying the total volume flow by the concentration of N₂O.

Statistical analysis is applied to both the baseline emissions factor and each campaign-specific project emissions factor. Only those N₂O measurements taken when the plant is operating within the permitted range will be considered in the calculation of baseline emissions. The level of uncertainty determined for the N₂O monitoring equipment will be deducted from the baseline emissions factor.

The project emissions factor is calculated as the ‘moving average’ of project emission factor of all the campaigns completed at that point in time. To determine the total emission reductions for a particular project campaign the project emissions factor is the higher of the following two values: (i) the moving average project emissions factor; and (ii) the project emission factor for that particular campaign. Also, to account for any N₂O emission reductions that may occur anyway as a consequence of potential platinum deposit build up inside the plant, the moving average factor is capped at the level of the lowest campaign specific emissions factor observed during the first 10 campaigns.

Selected approach from paragraph 48 of the CDM modalities and procedures

“Existing actual or historical emissions, as applicable”.

Applicability

This Baseline Methodology is applicable to project activities that install a secondary N₂O abatement catalyst inside the ammonia burner of a nitric acid plant, underneath the precious metal gauze pack. The methodology is applicable under the following conditions:

The applicability is limited to the existing production capacity measured in tonnes of nitric acid, where the commercial production had began no later than 31 December 2005. Definition of “existing” production capacity is applied for the process with the existing ammonia oxidization reactor where N₂O is generated and not for the process with new ammonia oxidizer. Existing production “capacity” is defined as the designed capacity, measured in tons of nitric acid per year.

The project activity will not result in the shut down of any existing N₂O destruction or abatement facility or equipment in the plant.

- The project activity shall not affect the level of nitric acid production;
- There are currently no regulatory requirements or incentives to reduce levels of N₂O emissions from nitric acid plants in the host country;
- The project activity will not increase NO_x emissions;



- NO_x abatement catalyst installed, if any, prior to the start of the project activity is not a Non-Selective Catalytic Reduction (NSCR) DeNO_x unit;
- Operation of the secondary N₂O abatement catalyst installed under the project activity does not lead to any process emissions of greenhouse gases, directly or indirectly;
- Continuous real-time measurements of N₂O concentration and total gas volume flow can be carried out in the stack:
 - Prior to the installation of the secondary catalyst for one campaign; and
 - After the installation of the secondary catalyst throughout the chosen crediting period of the project activity.

This Baseline Methodology shall be used in conjunction with the proposed new monitoring methodology AM0034 (“Catalytic reduction of N₂O inside the ammonia burner of nitric acid plants”).

II. BASELINE METHODOLOGY PROCEDURE

Identification of baseline scenario

The baseline scenario shall be identified using procedure for identification of the baseline scenario described in the approved methodology AM0028 “Catalytic N₂O destruction in the tail gas of nitric acid Plants”.

Additionality

The additionality of the project activity shall be demonstrated and assessed using the latest approved version of the “Tool for the demonstration and assessment of additionality” agreed by the Executive Board.

Because of the similarity of both approaches used to determine the baseline scenario and the additionality tool, Step 1 of the “Tool for the demonstration and assessment of additionality” may be omitted while assessing the additionality.

Consistency shall be ensured between the determination of the baseline scenario and the demonstration of additionality. The baseline scenario alternative selected in the previous section shall be used when applying Steps 2 to 5 of the “Tool for the demonstration and assessment of additionality”.

In the event of re-assessment of the baseline scenario as a consequence of new NO_x regulations over the course of the crediting period of the proposed project activity, the re-assessment of the baseline scenario shall be undertaken using the same 5-Step process mentioned above. In such a case the additionality of the project must be re-demonstrated.

Project Boundary

The spatial extent of the project boundary shall cover the facility and equipment for the complete nitric acid production process from the inlet to the ammonia burner to the stack. This includes all compressors, tail gas expander turbines and any NO_x abatement equipment installed. The only greenhouse gas to be included is the N₂O contained in the waste stream exiting the stack.

Flow diagrams of different types of nitric acid plants (high, medium and low pressure; mono and dual pressure; plant constructor) differ substantially. Therefore, a plant specific flow diagram should be



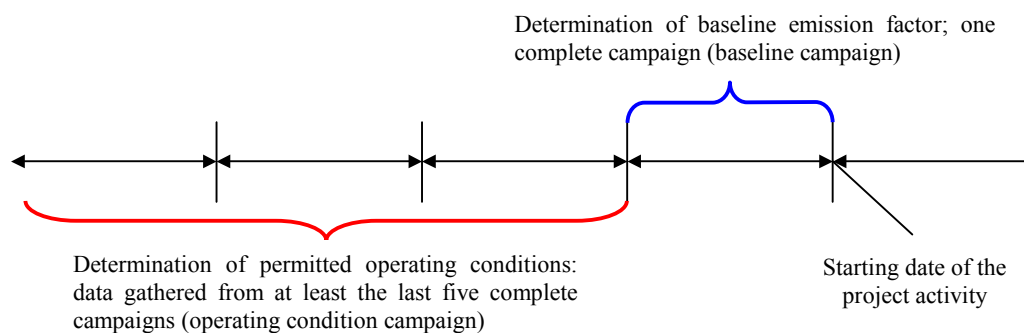
provided in the Project Design Document to demonstrate the project boundary of the particular nitric acid plants(s) involved in the project activity.

Table 1: Overview of emission sources included or excluded from the project boundary

	Source	Gas	Included?	Justification / Explanation
Baseline	Nitric Acid Plant (Burner Inlet to Stack)	CO ₂	Excluded	The project does not lead to any change in CO ₂ or CH ₄ emissions, and, therefore, these are not included.
		CH ₄	Excluded	
		N ₂ O	Included	
Project Activity	Nitric Acid Plant (Burner Inlet to Stack)	CO ₂	Excluded	The project does not lead to any change in CO ₂ or CH ₄ emissions
		CH ₄	Excluded	
		N ₂ O	Included	
	Leakage emissions from production, transport, operation and decommissioning of the catalyst.	CO ₂	Excluded	No leakage emissions are expected
		CH ₄	Excluded	
		N ₂ O	Excluded	

Baseline Emissions

The baseline shall be established through continuous monitoring of both N₂O concentration and gas flow volume in the stack of the nitric acid plant for one complete campaign prior to project implementation. The schematic of the procedure is as follows:



1. Determination of the permitted operating conditions of the nitric acid plant to avoid overestimation of baseline emissions

In order to avoid the possibility that the operating conditions of the nitric acid production plant are modified in such a way that increases N₂O generation during the baseline campaign, the normal ranges for operating conditions shall be determined for the following parameters: (i) oxidation temperature; (ii) oxidation pressure; (iii) ammonia gas flow rate, and (iv) air input flow rates. The permitted range shall be established using the procedures described below. Note that data for these parameters is routinely logged in the process control systems of the plant.



Oxidation temperature and pressure:

Process parameters to be monitored are the following:

- OT_h Oxidation temperature for each hour (°C);
- OP_h Oxidation pressure for each hour (Pa);
- OT_{normal} Normal range for oxidation temperature (°C);
- OP_{normal} Normal range for oxidation pressure (Pa).

The “permitted range” for oxidation temperature and pressure is to be determined using one of the following sources:

- (a) Historical data for the operating range of temperature and pressure from the previous five campaigns (or fewer, if the plant has not been operating for five campaigns); or, then
- (b) If no data on historical temperatures and pressures is available, the range of temperature and pressure stipulated in the operating manual for the existing equipment; or
- (c) If no operating manual is available or the operating manual gives insufficient information, from an appropriate technical literature source.¹

If option (a) is selected, the permitted range is determined through a statistical analysis of the historical data in which the time series data is to be interpreted as a sample for a stochastic variable. All data that falls within the upper and lower 2.5% percentiles of the sample distribution is defined as abnormal and shall be eliminated. The permitted range of operating temperature and pressure is then assigned as the historical minimum (value of parameter below which 2.5% of the observation lie) and maximum operating conditions (value of parameter exceeded by 2.5% of observations).

Ammonia gas flow rates and ammonia to air ratio input into the ammonia oxidation reactor (AOR):

Parameters to be monitored:

AFR	Ammonia gas flow rate to the AOR	(tNH ₃ /h);
AFR _{max}	Maximum ammonia gas flow rate to the AOR	(tNH ₃ /h);
AIFR ₋	Ammonia to air ratio	(%);
AIFR _{max_-}	Maximum ammonia to air ratio	(%).

The upper limits for ammonia flow and ammonia to air ratio shall be determined using one of the following three options, in preferential order:

- (a) Historical maximum operating data for hourly ammonia gas and ammonia to air ratio for the previous five campaigns (or fewer, if the plant has not been operating for five campaigns; excluding abnormal campaigns; or
- (b) If no data is available, calculation of the maximum permitted ammonia gas flow rates and ammonia to air ratio as specified by the ammonia oxidation catalyst manufacturer or for typical catalyst loadings; or
- (c) If information for (b) above is not available, based on a relevant technical literature source.

Once the permitted ranges for pressure, temperature, ammonia flow rate and ammonia to air ratio are determined, it must also be demonstrated that these ranges are within the specifications of the facility. If not, the baseline campaign must be reassessed.

¹ E.g. from Ullmann’s Encyclopedia of Industrial Chemistry, Fifth, completely revised edition, Volume A 17, VCH, 1991, P. 298, Table 3 or other standard reference work or literature source.

2. Determination of baseline emission factor: measurement procedure for N₂O concentration and gas volume flow

N₂O concentration and gas volume flow are to be monitored throughout the baseline campaign. The monitoring system is to be installed using the European Norm 14181² (2004) (Please refer Annex 1 for **Monitoring** practices and performance **standards to be followed**). This monitoring system provides separate readings for N₂O concentration and gas flow volume for a defined period of time (e.g., every hour of operation, it provides an average of the measured values for the previous 60 minutes). Error readings (e.g., downtime or malfunction) and extreme values are to be automatically eliminated from the output data series by the monitoring system.

Measurement results can be distorted before and after periods of downtime or malfunction of the monitoring system and can lead to mavericks. To eliminate such extremes and to ensure a conservative approach, the following statistical evaluation is to be applied to the complete data series of N₂O concentration as well as to the data series for gas volume flow. The statistical procedure will be applied to data obtained after eliminating data measured for periods where the plant operated outside the permitted ranges:

- (a) Calculate the sample mean (\bar{x});
- (b) Calculate the sample standard deviation(s);
- (c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation);
- (d) Eliminate all data that lie outside the 95% confidence interval;
- (e) Calculate the new sample mean from the remaining values (volume of stack gas (VSG) and N₂O concentration of stack gas (NCSG)).

The average mass of N₂O emissions per hour is estimated as product of the NCSG and VSG.³ The N₂O emissions per campaign are estimates product of N₂O emission per hour and the total number of complete hours of operation of the campaign using the following equation:

$$BE_{BC} = VSG_{BC} \times NCSG_{BC} \times OH_{BC} \times 10^{-9} \quad (\text{tN}_2\text{O}) \quad (1)$$

² Project proponents can use other comparable national or international standards, provided they demonstrate the comparability of the used standard/s with EN14181 in the CDM-PDD.

³ The baseline emission factor for N₂O per unit nitric acid production is estimated as estimated N₂O produced during the campaign divided by the total nitric acid produced during that campaign. The total N₂O produced is estimated and not measured, as N₂O production during the periods when the plant is operating outside the normal operating parameters can be greater than when it is operating within the normal operating period. N₂O produced in a campaign is estimated as product of average N₂O concentration in the stack gas, volume of stack gas for the campaign, and operating hours of the campaign. To ensure that N₂O is conservatively estimated, all the values of N₂O concentration in the stack gas and hourly flow rate of stack gas recorded when the plant is operating outside the normal parameters are excluded from estimating the average N₂O concentration and hourly flow rate values for the campaign. As the N₂O emission factor is calculated as estimated N₂O produced during the campaign divided by the actual nitric acid produced during the campaign, the estimated N₂O for campaign reflects the N₂O that would have been produced had the operating parameters of plant been within the normal operating range. Therefore, the total operating hours of the campaign are used in equation (1).

The plant specific baseline emissions factor representing the average N₂O emissions per tonne of nitric acid over one full campaign is derived by dividing the total mass of N₂O emissions by the total output of 100% concentrated nitric acid for that period. The overall uncertainty of the monitoring system shall also be determined and the measurement error will be expressed as a percentage (*UNC*). The N₂O emission factor per tonne of nitric acid produced in the baseline period (*EF_{BL}*) shall then be reduced by the estimated percentage error as follows:

$$EF_{BL} = \left(1 - \frac{UNC}{100}\right) \left(\frac{BE_{BC}}{NAP_{BC}}\right) \quad (\text{tN}_2\text{O}/\text{tHNO}_3) \quad (2)$$

Where:

- EF_{BL}* = Baseline N₂O emissions factor (tN₂O/tHNO₃)
- BE_{BC}* = Total N₂O emissions during the baseline campaign (tN₂O)
- NCSG_{BC}* = Mean concentration of N₂O in the stack gas during the baseline campaign (mgN₂O/m³)
- OH_{BC}* = Total operating hours of the baseline campaign (h)
- VSG_{BC}* = Mean gas volume flow rate at the stack in the baseline measurement period (m³/h)⁴
- NAP_{BC}* = Total nitric acid production during the baseline campaign (tHNO₃)
- UNC* = Overall uncertainty of the monitoring system (%), calculated as the combined uncertainty of the applied monitoring equipment

In the absence of any national or regional regulations for N₂O emissions, the resulting *EF_{BL}* will be used as the baseline emission factor.

Note: Under certain circumstances, the operating conditions during the measurement period used to determine baseline N₂O emission factor may be outside the permitted range or limit corresponding to normal operating conditions. For instance, temperature, pressure, ammonia flow rate or ammonia to air ratio may be outside the permitted condition. Any N₂O baseline data that is measured during hours where the operating conditions are outside the permitted range, except *OH_{BC}* and *NAP_{BC}*, must be eliminated from the calculation of the baseline emissions factor. If historical data and baseline data for each minute are available, values could be eliminated on a minute-by-minute basis.

The baseline campaign is not valid and must be repeated if the plant operates outside of the permitted range for more than 50% of the duration of the baseline campaign.

In order to further ensure that operating conditions during the baseline campaign are representative of normal operating conditions, statistical tests should be performed to compare the average values of the permitted operating conditions with the average values obtained during the baseline determination period. If it can be concluded with 95% confidence level, in any of the tests, that the two values are different, then the baseline determination should be repeated.

⁴ *VSG_{BC}* and *NCSG_{BC}* should be measured simultaneously, and values should be expressed on the same basis (wet or dry) and should be corrected to normal conditions (101.325 kPa, 0 deg C). If the instrument (or measurement system) uses an algorithm to convert actual conditions to normal conditions, the proper source of such an algorithm should be used (e.g., based on procedures of EN14181). For all the cases, either manual or algorithm-based conversion of actual conditions to normal conditions, the temperature and pressure of actual conditions of stack gas should be recorded as per monitoring plan of this methodology.



Impact of regulations

Should N₂O emissions regulations that apply to nitric acid plants be introduced in the host country or jurisdiction covering the location of the project activity, such regulations shall be compared to the calculated baseline factor for the project (EF_{BL}), regardless of whether the regulatory level is expressed as:

- An absolute cap on the total volume of N₂O emissions for a set period;
- A relative limit on N₂O emissions expressed as a quantity per unit of output; or
- A threshold value for specific N₂O mass flow in the stack.

In this case, a corresponding plant-specific emissions factor cap (max. allowed tN₂O/tHNO₃) is to be derived from the regulatory level. If the regulatory limit is lower than the baseline factor determined for the project, the regulatory limit shall serve as the new baseline factor, that is:

If $EF_{BL} > EF_{reg}$

Then the baseline N₂O emission factor shall be EF_{reg} for all calculations.

Where:

EF_{BL} = Baseline emissions factor (tN₂O/tHNO₃)

EF_{reg} = Emissions level set by newly introduced policies or regulations (tN₂O/tHNO₃). Such EF_{reg} shall be determined according to the nature of the regulation (e.g., in terms of absolute emission, by-product rate, concentration in stack gas), as described in the approved methodology AM0028

Composition of the ammonia oxidation catalyst

If the composition of the ammonia oxidation catalyst used for the baseline campaign and after the implementation of the project are identical to that used in the campaign for setting the operating conditions (previous five campaigns), then there shall be no limitations on N₂O baseline emissions.

A change in the composition of the ammonia oxidation catalyst in the baseline campaign to a composition other than that used in the previous five campaigns, is permissible without any limitation on the N₂O baseline emissions if the following conditions are met:

- (i) The baseline catalyst composition is considered as common practice in the industry; or
- (ii) The change in catalyst composition is justified by its availability, performance, relevant literature etc.

Otherwise, the baseline emission factor shall be set to the conservative IPCC default emission factor for N₂O from nitric acid plants which have not installed N₂O destruction measures (4.5 kg-N₂O/t HNO₃).



If the nitric acid plant operator has changed the composition of the ammonia oxidation catalyst in a project campaign to a composition not used in the baseline campaign, the project proponent could:

- (i) Repeat the baseline campaign to determine a new baseline emissions factor ($tN_2O/tHNO_3$), compare it to the previous baseline emissions factor and adopt the lower figure as EF_{BL} , or
- (ii) Set the baseline emissions factor to the conservative IPCC default emission factor for N_2O from nitric acid plants which have not installed N_2O destruction measures ($4.5 \text{ kg-}N_2O/t \text{ HNO}_3$).

Parameters to be monitored for composition of the catalyst are as follows:

GS_{normal}	Gauze supplier for the operation condition campaigns;
GS_{BL}	Gauze supplier for baseline campaign;
$GS_{project}$	Gauze supplier for the project campaign;
G_{normal}	Gauze composition for the operation condition campaigns;
GC_{BL}	Gauze composition for baseline campaign;
$GC_{project}$	Gauze composition for the project campaign.

Campaign Length

In order to take into account the variations in campaign length and its influence on N_2O emission levels, the historic campaign lengths and the baseline campaign length are to be determined and compared to the project campaign length. Campaign length is defined as the total number of metric tonnes of nitric acid at 100% concentration produced with one set of gauzes.

Historic Campaign Length

The average historic campaign length (CL_{normal}) defined as the average campaign length for the historic campaigns used to define operating condition (the previous five campaigns), will be used as a cap on the length of the baseline campaign.

Baseline Campaign Length (CL_{BL})

If $CL_{BL} \leq CL_{normal}$ All N_2O values measured during the baseline campaign can be used for the calculation of EF_{BL} (subject to the elimination of data that was monitored during times where the plant was operating outside of the “permitted range”).

If $CL_{BL} > CL_{normal}$ N_2O values that were measured beyond the length of CL_{normal} during the production of the quantity of nitric acid (i.e. the final tonnes produced) are to be eliminated from the calculation of EF_{BL} .

Project Emissions

Over the duration of the project activity, N_2O concentration and gas volume flow in the stack of the nitric acid plant as well as the temperature and pressure of ammonia gas flow and ammonia-to-air ratio, will be measured continuously.

Estimation of campaign-specific project emissions

The monitoring system is to be installed using the guidance document EN 14181 and will provide separate readings for N₂O concentration and gas flow volume for a defined period of time (e.g., every hour of operation, i.e., an average of the measuring values of the past 60 minutes). Error readings (e.g. downtime or malfunction) and extreme values are automatically eliminated from the output data series by the monitoring system. Next, the same statistical evaluation that was applied to the baseline data series is to be applied to the project data series:

- (a) Calculate the sample mean (\bar{x});
- (b) Calculate the sample standard deviation(s);
- (c) Calculate the 95% confidence interval (equal to 1.96 times the standard deviation);
- (d) Eliminate all data that lie outside the 95% confidence interval;
- (e) Calculate the new sample mean from the remaining values.

$$PE_n = VSG \times NCSG \times OH \times 10^{-9} \quad (\text{tN}_2\text{O}) \quad (3)$$

Where:

- VSG = Mean stack gas volume flow rate for the project campaign (m³/h)⁵
 $NCSG$ = Mean concentration of N₂O in the stack gas for the project campaign (mgN₂O/m³)
 PE_n = Total N₂O emissions of the nth project campaign (tN₂O)
 OH = Is the number of hours of operation in the specific monitoring period (h)

Derivation of a moving average emission factor

In order to take into account possible long-term emissions trends over the duration of the project activity and to take a conservative approach a moving average emission factor shall be estimated as follows:

Step 1: Estimate campaign specific emissions factor for each campaign during the project's crediting period by dividing the total mass of N₂O emissions during that campaign by the total production of 100% concentrated nitric acid during that same campaign

For example, for campaign 'n' the campaign specific emission factor would be:

$$EF_n = PE_n / NAP_n \quad (\text{tN}_2\text{O}/\text{tHNO}_3) \quad (4)$$

Step 2: Estimate a moving average emissions factor be calculated at the end of a campaign 'n' as follows:

$$EF_{ma,n} = (EF_1 + EF_2 + \dots + EF_n) / n \quad (\text{tN}_2\text{O}/\text{tHNO}_3) \quad (5)$$

⁵ VSG_{BC} and NCSG_{BC} should be measured simultaneously, and values should be expressed on the same basis (wet or dry) and should be corrected to normal conditions (101.325 kPa, 0 deg C). If the instrument (or measurement system) uses the algorithm to convert actual conditions to normal conditions, the proper source of such algorithm should be used (e.g. based on procedures of EN14181). For all the cases, either manual or algorithm-based conversion of actual conditions to normal conditions, the temperature and pressure of actual conditions of stack gas should be recorded as per monitoring plan of this methodology.



This process is repeated for each campaign such that a moving average, $EF_{ma,n}$, is established over time, becoming more representative and precise with each additional campaign.

To calculate the total emission reductions achieved in a campaign in formula (7) below, the higher of the two values $EF_{ma,n}$ and EF_n shall be applied as the emission factor relevant for the particular campaign to be used to calculate emissions reductions (EF_p). Thus:

$$\text{If } EF_{ma,n} \geq EF_n, \text{ then } EF_p = EF_{ma,n} \quad (6)$$

$$\text{If } EF_{ma,n} < EF_n, \text{ then } EF_p = EF_n$$

Where:

EF_n	=	Emission factor calculated for a specific project campaign (tN ₂ O/tHNO ₃)
$EF_{ma,n}$	=	Moving average (ma) emission factor of after n th campaigns, including the current campaign (tN ₂ O/tHNO ₃)
n	=	Number of campaigns to date
EF_p	=	Emissions factor that will be applied to calculate the emissions reductions from this specific campaign (i.e., the higher of EF_x and EF_n) (N ₂ O/tHNO ₃)

Minimum project emission factor

A campaign-specific emissions factor shall be used to cap any potential long-term trend towards decreasing N₂O emissions that may result from a potential built up of platinum deposits. After the first ten campaigns of the crediting period of the project, the lowest EF_n observed during those campaigns will be adopted as a minimum (EF_{min}). If any of the later project campaigns results in a EF_n that is lower than EF_{min} , the calculation of the emission reductions for that particular campaign shall use EF_{min} and not EF_n .⁶

Where:

EF_{min}	=	Is equal to the lowest EF_n observed during the first 10 campaigns of the project crediting period (N ₂ O/tHNO ₃)
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Project Campaign Length

(a) Longer Project Campaign

If the length of each individual project campaign CL_n is longer than or equal to the average historic campaign length CL_{normal} , then all N₂O values measured during the project campaign can be used for the calculation of EF (subject to the elimination of data from the Ammonia/Air analysis, see above);

⁶ In practice this will mean that, if the assumption that platinum deposits do have a reducing effect on N₂O emissions is correct, then an increasing adoption of EF_{min} instead of EF_n should be experienced as the project progresses through its crediting period.

**(b) Shorter Project Campaign**

If $CL_n < CL_{normal}$, recalculate EF_{BL} by eliminating those N_2O values that were obtained during the production of tonnes of nitric acid beyond the CL_n (i.e. the last tonnes produced) from the calculation of EF_n .

Leakage

No leakage calculation is required.

Emission Reductions

The emission reductions for the project activity over a specific campaign are determined by deducting the campaign-specific emission factor from the baseline emission factor and multiplying the result by the production output of 100% concentrated nitric acid over the campaign period and the GWP of N_2O :

$$ER = (EF_{BL} - EF_p) \times NAP \times GWP_{N_2O} \quad (\text{tCO}_2\text{e}) \quad (7)$$

Where:

ER	=	Emission reductions of the project for the specific campaign (tCO ₂ e)
NAP	=	Nitric acid production for the project campaign (tHNO ₃). The maximum value of NAP shall not exceed the design capacity
EF_{BL}	=	Baseline emissions factor (tN ₂ O/tHNO ₃)
EF_p	=	Emissions factor used to calculate the emissions from this particular campaign (i.e., the higher of $EF_{ma,n}$ and EF_n)
GWP_{N_2O}	=	Global warming potential for the N_2O as per IPCC default value

By nameplate (design) implies the total yearly capacity (considering 365 days of operation per year) as per the documentation of the plant technology provider (such as the Operation Manual). If the plant has been modified to increase production, and such de-bottleneck or expansion projects were completed before December 2005, then the new capacity is considered nameplate, provided proper documentation of the projects is available (such as, but not limited to: properly dated engineering plans or blueprints, engineering, materials and/or equipment expenses, or third party construction services, etc.).

Changes required for methodology implementation in 2nd and 3rd crediting periods

No changes are required.

Data and parameters not monitored

In addition to the parameters listed in the tables below, the provisions on data and parameters not monitored in the tools referred to in this methodology apply.



The following items are demanded to confirm applicability conditions:

ID Number:	B.1
Parameter:	AFR_{max}
Data unit:	kgNH ₃ /h
Description:	Maximum ammonia flow rate
Source of data:	Plant records
Measurement procedures (if any):	
Any comment:	Information available in electronic records and paper for at least 2 years

ID Number:	B.2
Parameter:	$AIFR_{max}$
Data unit:	m ³ /h
Description:	Maximum ammonia to air ratio
Source of data:	Calculated
Measurement procedures (if any):	
Any comment:	Information available in electronic records and paper for at least 2 years

ID Number:	B.3
Parameter:	OT_{normal}
Data unit:	°C
Description:	Normal operating temperature
Source of data:	Historical monitoring
Measurement procedures (if any):	
Any comment:	Information available in electronic records and paper for at least 2 years

D Number:	B.4
Parameter:	OP_{normal}
Data unit:	Pa
Description:	
Source of data:	
Measurement procedures (if any):	
Any comment:	Information available in electronic records and paper for at least 2 years



ID Number:	B.5
Parameter:	GS _{BL}
Data unit:	Nil
Description:	Gauze supplier for the baseline campaign
Source of data:	Monitored
Measurement procedures (if any):	
Any comment:	To be obtained during the baseline campaign. The information will be stored in electronic records and paper for the crediting period

ID Number:	B.6
Parameter:	GC _{BL}
Data unit:	
Description:	Gauze composition during baseline campaign
Source of data:	Monitored
Measurement procedures (if any):	
Any comment:	To be obtained during the baseline campaign. The information will be stored in electronic records and paper for the crediting period

III. MONITORING METHODOLOGY

This monitoring methodology requires the collection of historic N₂O emissions baseline data and the monitoring of ammonia and air input and pressure and temperature inside the ammonia burner during one production campaign of the nitric acid plant prior to the installation of the N₂O abatement catalyst, as well as the continued monitoring of the N₂O emissions after the installation of the N₂O abatement catalyst.

The Automated Measuring System (AMS) consisting of the following shall be used for monitoring:

- An automated extractive gas analyzer system that uses Non Dispersive Infrared Absorption (NDIR) (including probes, pipes and sample conditioning system) that will continuously measure (as per required frequency i.e., every 2 seconds) the concentration of N₂O in the stack gas of the nitric acid plant. A probe extracts the homogenously mixed gas directly from the stack or tail gas stream from the point at which it is pumped through gas lines to the analyzer; or
- An in-situ analyser that will continuously measure (as per required frequency i.e. every 2 seconds) the concentration of N₂O in the stack gas of the nitric acid plant; and
- A gas volume flow meter that uses either pressure-differential or ultrasonic techniques to continuously monitor the gas volume flow, temperature and pressure, in the stack of the nitric acid plant.

If pressure-differential technology is applied, sampling shall be carried out continuously using a multiple-point sampling tube that is optimized to the specific width and height of the stack, and the expected gas velocities in the stack.



Temperature and pressure in the stack will also be measured continuously and used to calculate the gas volume flow at the prescribed temperature and pressure. This calculation of gas volume flow at standard conditions will be carried out automatically by the AMS.

In addition, the total production of nitric acid and the number of operating hours will be recorded.

A plant specific emissions factor will be calculated from the monitored data, both during the baseline period and for each production campaign of the project activity. Statistical evaluation is applied in order to eliminate distortions in these emissions factors.

Quality assurance tests and annual functional test for the Automated Measuring Systems (including SRM measurements) are recommended regarding the selection, installation, configuration and operation of the Automated Measuring Systems. Application of ability tested Automated Measuring System. Calculation of Automated Measuring System uncertainty. Maintenance checks and regular calibrations according to vendor specifications standards. It is recommended that main spare parts be kept on -site to guarantee optimum uptime performance. Weekly and monthly service and maintenance should be performed by the user following instructions during the commissioning phase. The vendor will undertake annual Service. Technical Support avoids downtimes and comprise of local back up through service agent including maintenance and re-commissioning if necessary. Moreover, full field and workshop support, hot-line technical telephone and online support. It is recommended to address Quality Control by having an independent validator on site for the calibration of the monitoring equipment and system during the commissioning phase.

In the selection of downstream measuring points the following issues have to be considered: temperature of the gas below 300°C (N₂O inert), assurance of homogeneity of the volume gas flow at the measuring points throughout the diameter in terms of velocity of flow and mass composition of gas flow, possible turbulences in the gas flow stream (e.g., at the stack walls), if in-homogeneities exist, measuring of the gas flow has to be conducted with specific measuring equipment that minimizes uncertainties and non-homogeneities to a minimum (e.g., multiple probe measuring units that allow for a representative coverage of the gas flow across the stack diameter). It is recommended that the measuring points be placed at points with the plant with easy access behind the gas expander turbine where the gas flow streams are consistent.

Measurement uncertainties that could occur by applying continuous online measurement upstream of the secondary catalyst are avoided from the beginning (Heterogeneity of gas composition; Space constraints and gas leaks; Corrosion due to acidic environment; Downstream reactions).

**Data and parameters monitored**

Data / Parameter:	NCSG
Data unit:	mgN ₂ O/m ³ at normal conditions (101.325 kPa, 0 deg C) (converted from ppm if necessary)
Description:	N ₂ O concentration in the stack gas
Source of data:	N ₂ O analyser
Measurement procedures (if any):	
Monitoring frequency:	Every 2 seconds
QA/QC procedures:	Regular calibrations according to vendor specifications and recognised industry standards (EN 14181). Staff will be trained in monitoring procedures and a reliable technical support infrastructure will set up
Any comment:	The data output from the analyser will be processed using appropriate software program. The information will be stored in electronic records and paper for at least 2 years

Data / Parameter:	VSG
Data unit:	m ³ /h
Description:	Volume flow rate of the stack gas. It should be expressed in normal conditions (101.325 kPa, 0 deg C)
Source of data:	Gas volume flow meter
Measurement procedures (if any):	
Monitoring frequency:	Every 2 seconds
QA/QC procedures:	Regular calibrations according to vendor specifications and recognised industry standards (EN 14181). Staff will be trained in monitoring procedures and a reliable technical support infrastructure will set up
Any comment:	The data output from the stack flow meter will be processed using appropriate software. The information will be stored in electronic records and paper for at least 2 years

Data / Parameter:	OH
Data unit:	Hours
Description:	Operating hours
Source of data:	Production log
Measurement procedures (if any):	
Monitoring frequency:	Daily, compiled for entire campaign
QA/QC procedures:	Included in evaluation by third party validator
Any comment:	Plant manager records the hours of full operation of the plant during a campaign. The information will be stored in electronic records and paper for at least 2 years



Data / Parameter:	NAP
Data unit:	tHNO ₃
Description:	Nitric Acid production (100% concentrate)
Source of data:	Production log
Measurement procedures (if any):	
Monitoring frequency:	Daily, compiled for entire campaign
QA/QC procedures:	Included in evaluation by third party validator
Any comment:	Total production over project campaign. The information will be stored in electronic records and paper for at least 2 years

Data / Parameter:	TSG
Data unit:	°C
Description:	Temperature of the stack gas
Source of data:	Probe (part of gas volume flow meter)
Measurement procedures (if any):	
Monitoring frequency:	Every 2 seconds
QA/QC procedures:	Regular calibrations according to vendor specifications and recognised industry standards (EN 14181). Staff will be trained in monitoring procedures and a reliable technical support infrastructure will set up
Any comment:	The information will be stored in electronic records and paper for at least 2 years

Data / Parameter:	PSG
Data unit:	Pa
Description:	Pressure of stack gas
Source of data:	Probe (part of gas volume flow meter)
Measurement procedures (if any):	
Monitoring frequency:	Every 2 seconds
QA/QC procedures:	Regular calibrations according to vendor specifications and recognised industry standards (EN 14181). Staff will be trained in monitoring procedures and a reliable technical support infrastructure will set up
Any comment:	The information will be stored in electronic records and paper for at least 2 years



Data / Parameter:	NCSG _{BC}
Data unit:	
Description:	N ₂ O concentration in the stack gas at normal conditions (101.325 kPa, 0 deg C).
Source of data:	N ₂ O analyser
Measurement procedures (if any):	
Monitoring frequency:	Every 2 seconds
QA/QC procedures:	Regular calibrations according to vendor specifications and recognised industry standards (EN 14181). Staff will be trained in monitoring procedures and a reliable technical support infrastructure will set up
Any comment:	The data output from the analyser will be processed using appropriate software. The information will be stored in electronic records and paper for the entire crediting period

Data / Parameter:	VSG _{BC}
Data unit:	m ³ /h
Description:	Volume flow rate of the stack gas. It should be expressed in normal conditions (101.325 kPa, 0 deg C)
Source of data:	Gas volume flow meter
Measurement procedures (if any):	
Monitoring frequency:	Every 2 seconds
QA/QC procedures:	Regular calibrations according to vendor specifications and recognised industry standards (EN 14181). Staff will be trained in monitoring procedures and a reliable technical support infrastructure will set up
Any comment:	The data output from the stack flow meter will be processed using appropriate software. The information will be stored in electronic records and paper for the entire crediting period

Data / Parameter:	OH _{BC}
Data unit:	Hours
Description:	Operating hours
Source of data:	Production log
Measurement procedures (if any):	
Monitoring frequency:	Daily, compiled for entire campaign
QA/QC procedures:	Included in evaluation by third party validator
Any comment:	Plant manager records the hours of full operation of the plant during a campaign. The information will be stored in electronic records and paper for the entire crediting period



Data / Parameter:	NAP _{BC}
Data unit:	tHNO ₃
Description:	Nitric acid (100% concentrated) over baseline campaign
Source of data:	Production log
Measurement procedures (if any):	
Monitoring frequency:	Daily, compiled for entire campaign
QA/QC procedures:	Included in evaluation by third party validator
Any comment:	The information will be stored in electronic records and paper for the entire crediting period

Data / Parameter:	AFR
Data unit:	kgNH ₃ /h
Description:	Ammonia gas flow rate to the AOR
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	Continuously
QA/QC procedures:	Included in evaluation by third party validator
Any comment:	To be obtained from the operating condition campaign. The information will be stored in electronic records and paper for at least 2 years

Data / Parameter:	UNC
Data unit:	%
Description:	Overall measurement uncertainty of the monitoring system
Source of data:	Calculation of the combined uncertainty of the applied monitoring equipment
Measurement procedures (if any):	
Monitoring frequency:	Once after monitoring system is commissioned
QA/QC procedures:	
Any comment:	The information will be stored in electronic and paper for the duration of the project activity



Data / Parameter:	AIFR
Data unit:	m ³ /h
Description:	Ammonia to air ratio
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	Every hour
QA/QC procedures:	
Any comment:	To be obtained from the operating condition campaign. The information will be stored in electronic and paper for at least 2 years

Data / Parameter:	CL _{BL}
Data unit:	tHNO ₃
Description:	Length of the baseline campaign
Source of data:	Calculated from nitric acid production data
Measurement procedures (if any):	
Monitoring frequency:	After the end of each campaign
QA/QC procedures:	
Any comment:	The information will be stored in electronic and paper for at least 2 years

Data / Parameter:	CL _{normal}
Data unit:	tHNO ₃
Description:	Normal campaign length
Source of data:	Calculated from nitric acid production data
Measurement procedures (if any):	
Monitoring frequency:	Prior to end of baseline campaign
QA/QC procedures:	
Any comment:	Average historical campaign length during the operation condition campaigns



Data / Parameter:	OT _h
Data unit:	°C
Description:	Oxidation temperature for each hour
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	Every hour
QA/QC procedures:	
Any comment:	To be obtained from the operating condition campaign. The information will be stored in electronic records and paper for at least 2 years

Data / Parameter:	OP _h
Data unit:	Pa
Description:	Oxidation Pressure for each hour
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	Every hour
QA/QC procedures:	
Any comment:	To be obtained from the operating condition campaign. The information will be stored in electronic records and paper for at least 2 years

Data / Parameter:	GS _{normal}
Data unit:	
Description:	Normal gauze supplier for the operation condition campaigns
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	Each campaign
QA/QC procedures:	
Any comment:	To be obtained during the operating condition campaign. The information will be stored in electronic records and paper for the crediting period



Data / Parameter:	GS _{project}
Data unit:	
Description:	Gauze supplier for the project campaigns
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	Each campaign
QA/QC procedures:	
Any comment:	To be obtained during the project campaign. The information will be stored in electronic records and paper for the crediting period

Data / Parameter:	GC _{normal}
Data unit:	
Description:	Gauze composition during the operation campaign
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	Each campaign
QA/QC procedures:	
Any comment:	To be obtained during the operating condition campaign. The information will be stored in electronic records and paper for the crediting period

Data / Parameter:	GS _{BL}
Data unit:	
Description:	Gauze supplier for baseline campaign
Source of data:	Monitored
Measurement procedures (if any):	For project crediting period
Monitoring frequency:	
QA/QC procedures:	
Any comment:	To be obtained during the project campaign



Data / Parameter:	GC_{project}
Data unit:	
Description:	Gauze composition during baseline campaign
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	
QA/QC procedures:	
Any comment:	To be obtained during the project campaign. The information will be stored in electronic records and paper for the crediting period

Data / Parameter:	EF_{reg}
Data unit:	
Description:	Emissions level set by incoming policies or regulations
Source of data:	Monitored
Measurement procedures (if any):	
Monitoring frequency:	Updated when new regulations comes into force
QA/QC procedures:	
Any comment:	

IV. REFERENCES AND ANY OTHER INFORMATION

Not applicable.



Annex 1: **Monitoring practices and performance standards to be followed**

The accuracy of the N₂O emissions monitoring results is to be ensured by installing a monitoring system that has been certified to meet (or exceed) the requirements of the prevailing best industry practice or monitoring standards in terms of operation, maintenance and calibration. The latest applicable European standards and norms (EN 14181) shall be used as the basis for selecting and operating the monitoring system. **Project proponents can use other comparable national or international standards, provided they demonstrate the comparability of the used standard/s with EN14181 in the CDM-PDD.**

The following guidance documents are recommended as references for the Quality Assurance and Control procedures:

- (a) European Standard, Technical Committee Air Quality: Working Document, Air quality – Certification of automated measuring systems (AMS). Part 3: Performance specifications and test procedures for AMS for monitoring emissions from stationery sources, prEN 264022, CEN/TC 264:2005/1;
- (b) European Norm EN 14181: Quality assurance of automated measuring systems, 2004;
- (c) Bundesministerium für Umwelt, Naturschutz und Reaktorsicherheit (BMU), German Federal Ministry for the Environment, Nature Conservation and Nuclear Safety: Bundeseinheitliche Praxis bei der Überwachung der Emissionen. RdSchr. d. BMU v. 13.06.2005 – IG 12 – 45053/5.

The European Norm EN 14181 stipulates three levels of quality assurance tests and one annual functional test for Automated Measuring Systems, which are recommended to be used as guidance regarding the selection, installation and operation of the Automated Measuring Systems under this Monitoring Methodology:

- (1) Application of tested Automated Measuring System (evaluation according to DIN EN ISO 14956). Calculation of Automated Measuring System uncertainty before installation according to EN ISO 14956 including:
 - (a) Standard deviation;
 - (b) Lack of fit (linearity);
 - (c) Repeatability at zero and reference points;
 - (d) Time-dependent zero and span drift;
 - (e) Temperature dependence;
 - (f) Voltage fluctuation;
 - (g) Suitability test;
 - (h) Cross sensitivity to likely components of the stack gas;
 - (i) Influence of variations in flow rate on extractive Automated Measuring Systems;
 - (j) Response time;
 - (k) Detection limit;
 - (l) Influence of ambient conditions on zero and span readings;
 - (m) Performance and accuracy;
 - (n) Availability;
 - (o) Susceptibility to physical disturbances.

The specific performance characteristics of the monitoring system chosen by the project shall be listed in the Project Design Document. Also, project activities should calculate and show the margins of error for each of the performance characteristics as well as the cumulative error for the complete measuring system.



Installation and Calibration of the Automated Measuring System according to the Standard Reference Measurement Method (SRM), determination of the measurement uncertainty/variability of the Automated Measuring System and inspection of the compliance with the prescribed measurement uncertainties.

- (a) Selection of the location of measurement;
- (b) Duly installation of the monitoring equipment;
- (c) Correct choice of measurement range;
- (d) Calibration of the Automated Measuring System using the Standard-Reference-Method (SRM) as guidance;
- (e) Calibration curve either as linear regression or as straight line from absolute zero to centre of a scatter-plot;
- (f) Calculation of the standard deviation at the 95% confidence interval;
- (g) Inspection every three years;

Continuous quality assurance through the local operator/manager (drift and accuracy of the Automated Measuring System, verification management and documentation).

- (h) Permanent quality assurance during the plant operation by the operating staff;
- (i) Assurance of reliable and correct operation of the monitoring equipment (maintenance evidence);
- (j) Regular controls: zero point, span, drift, meet schedule of manufacturer maintenance intervals;

Annual functionality test including SRM measurements to check for uncertainties in the data measured by the Automated Measuring System.

- (k) Annual confirmation of the calibration curve;
- (l) Validity proof of calibration curves;
- (m) Back setting of excess meter of invalid calibration range;

EN 14181 prescribes which features Automated Measuring Systems need and how they are to be calibrated and maintained. The data resulting from the calibration experiment determine the calibration function as well as the measurement uncertainty and play the decisive role regarding the continuous monitoring of the measured data.

Minimum requirements for electronic evaluation units

- (n) Evaluation unit needs to take into account registration, mean average determination, validation, and evaluation;
- (o) The system and concept of emission data processing needs to be described;
- (p) Protocols and out-prints are required.

Downtime of Automated Measuring System

In the event that the monitoring system is down, the lowest between the conservative IPCC (4.5 kg N₂O / ton nitric acid) or the last measured value will be valid and applied for the downtime period for the baseline emission factor, and the highest measured value in the campaign will be applied for the downtime period for the campaign emission factor.



Data Sources

Association Française de Normalisation (AFNOR): Official standard for measuring and quantifying N₂O emissions in nitric acid plants, 2003.

Bundesministerium für Umwelt, Naturschutz und Reaktorsicherheit (BMU): Bundeseinheitliche Praxis bei der Überwachung der Emissionen. RdSchr. d. BMU v. 13.06.2005 – IG 12 – 45053/5. German Federal Ministry for the Environment, Nature Conservation and Nuclear Safety: Federal Standard Practice of Emission Monitoring, BMU, 2005.

European Norm EN 14181: Quality assurance of automated measuring systems, 2004.

European Standard, Technical Committee Air Quality: Working Document, Air quality – Certification of automated measuring systems (AMS). Part 3: Performance specifications and test procedures for AMS for monitoring emissions from stationery sources, prEN 264022, CEN/TC 264:2005/1.

European Fertilizers Manufacturers Association (EFMA): Best Available Techniques for Pollution Prevention and Control in the European Fertilizer Industry (Booklet No. 2 of 8) “PRODUCTION OF NITRIC ACID”, 2000.

European Fertilizer Manufacturers (EFMA): “The European Fertilizer Manufacturers’ Position on the European Commission’s Proposal for a Directive on EU Emissions Trading”, March 2005.

GHG Protocol <www.ghgprotocol.org>: “Calculating N₂O Emissions from the Production of Nitric Acid” Guide to calculation worksheets, October 2001.

Intergovernmental Panel on Climate Change (IPCC): “Default Factors for N₂O from Nitric Acid Production”, 2002.

Integrated Pollution Prevention and Control (IPPC): “Good Practice Guidance and Uncertainty Management in National Greenhouse Gas Inventories – N₂O Emissions from Adipic Acid and Nitric Acid Production”. Author Heike Mainhardt, ICF Inc, 2000.

Ruffer, A. von: Personal communication between GIAP, JSC Research and Development Institute of Nitrogen Industry and Organic Synthetic Products, Russia, and Albrecht von Ruffer, N.serve GmbH, on Russian nitric acid plant types and related N₂O emission levels, 2005.

Ruffer, A. von, Velsen-Zerweck, M. von: Personal communication between Johnson Matthey, dep. Noble Metals and Albrecht von Ruffer, Marten von Velsen-Zerweck, N.serve Environmental Services GmbH, on “Experience with measurements of N₂O concentrations inside ammonia burners”, 2005.

Marzo, L. M.: “Nitric Acid Production and Abatement Technology Including Azeotropic Acid”, The International Fertilizer Society, Proceedings No. 540, 2004.

Schwefer, M., Maurer, R., Groves, M.: “Reduction of Nitrous Oxide Emissions from Nitric Acid Plants”, Proceedings of Nitrogen 2000 in Vienna, 2000.

World Business Council for Sustainable Development (WBCSD): <www.ghgprotocol.org>, September 18 2005.



History of the document

Version	Date	Nature of revision(s)
03.3	EB 48, Annex 7 17 July 2009	Editorial revision to: <ul style="list-style-type: none">• Include in-situ analyser in the Automated Measuring System for measurement of N₂O concentration in stack gas;• Change in the name of Annex 1;• Clarifying that project proponents can use other comparable national or international standards, provided they demonstrate the comparability of the used standard/s with EN14181 in the CDM-PDD.
03.2	24 November 2008	Editorial revision to correct a typo in the paragraph of "Project Campaign Length".
03.1	EB 41, Annex 9 02 August 2008	Editorial revision to add footnote-3 and footnote-4 to clarify that volume of gas and N ₂ O concentration should be measured simultaneously and at same basis (wet or dry) and should be expressed at the normal conditions. The clarification made in the monitoring tables of these parameters also.
03	EB 38, Annex 3 14 March 2008	Clarification provided on the reason not to eliminate variables of Nitric Acid Production and Operational Hours of plant from calculation of N ₂ O baseline emission factor, when operating parameters are out of permitted range.
02	EB 27, Annex 5 01 November 2006	Definition inserted for facilities installed no later than 31 December.
01	EB 25, Annex 4 21 July 2006	Initial adoption.
Decision Class: Regulatory Document Type: Standard Business Function: Methodology		